

Theory and Technology of the Phosphorus Extraction from Ferrophosphorus

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Abstract

This article contains the research results of thermodynamic modelling of the chemical interaction of iron phosphides (Fe_3P , Fe_2P , FeP and FeP_2) with ferrosilicon FeSi_2 . The results were received by a method of the full thermodynamic analysis using the program HSC-5.1 of the Finnish metallurgical company Outokumpu, which was developed on a principle of the Gibbs energy minimization. The article considers the experimental results concerning to kinetics of the phosphorus extraction from electrothermal ferrophosphorus using ferrosilicon of a grade FS65. In addition, optimum technological parameters of the phosphorus extraction from the industrial ferrophosphorus, containing 26,4 % of phosphorus, and manufacture of a ferroalloy were determined.

Keywords: iron phosphides, ferrophosphorus, iron silicides, thermodynamic modelling, kinetics, ferrosilicon, phosphorus

1. Introduction

At the electrothermal production of yellow phosphorus from a phosphorite, quartzite and coke mixture, 1 ton of the phosphorus produced gives to 300 kg of a by-product – ferrophosphorus (1). The basic consumer of ferrophosphorus is the ferrous metallurgy, in which ferrophosphorus is used for melting of alloyed phosphorus-containing steels (for example, automatic steels), and iron casting. However, despite the introduction of (2) on industrial enterprises, a firm demand on the electrothermal ferrophosphorus has decreased recently because of chemical heterogeneity of the ferrophosphorus concerning to P, Mn, Si and the presence of slag inclusions in it (3). In connection with this, there is a necessity of development of a rational method of the electrothermal ferrophosphorus processing for manufacturing marketable products. The uniqueness of ferrophosphorus (as a raw material) is connected with a high phosphorus content – in 2-2,5 times more than in phosphorites.

In the world practice there are several directions of the ferrophosphorus processing (3-14). However, known methods of the ferrophosphorus processing have essential technological and economic disadvantages. So, phosphatic slags produced from ferrophosphorus are characterized by insufficient agrochemical activity, poor solubility in water owing to the presence of phosphorus in acid-soluble or citrate-soluble forms, therefore they have a limited application field. The technology of alkaline metals phosphates is much more complex, than the phosphatic slag technology, and a cost price of the products is higher. At the ferrophosphorus chlorination there are the problems concerning to the phosphorus chlorides purification from Si, Ti, V. Methods of the ferrophosphorus processing with production of P_2O_5 and phosphoric acid (processing by water steam, nitric acid, sulfuric acid, quartzite) are characterized by the nitrogen (II) oxide liberation, a low efficiency of sulfuric acid, a necessity of high pressure application, collateral formation of SO_2 , a low degree of the phosphorus conversion in P_2O_5 . The obtaining P_2O_3 from ferrophosphorus is complicated by the iron phosphate formation. The manufacture of element phosphorus and ferrosilicon from ferrophosphorus is characterized by a high power consumption connected with a necessity of preliminary reduction of Si from SiO_2 by carbon or with using the expensive technical silicon. The ferrophosphorus processing on phosphorus pentasulphide with further production of orthophosphoric acid is a multiphase manufacture demanding the cleaning phosphorus pentasulphide and leading to nonutilizable wastes and additional power inputs. The heating ferrophosphorus in vacuum even at 1600-1650 °C and low residual pressure allow taking the phosphorus no more 75 %. The ferrophosphorus processing in the presence of aluminium passes not up to the end and is accompanied by

formation of an intermediate Fe_3P , in addition, at the hydrolysis of AIP a poisonous phosphine is liberated.

At the development of a rational way of the ferrophosphorus processing we chose as a basis the ability of silicon to displace phosphorus from an iron phosphide melt. The given article contains the research results in the field of theory and technology of phosphorus extraction from iron phosphides and industrial ferrophosphorus in the presence of FeSi_2 and ferrosilicon of the grade FS65.

2. Research Method

Thermodynamic research of the chemical interaction of iron phosphides with ferrosilicon was carried out using the program HSC-5.1 of the Finnish metallurgical company Outokumpu, which was developed on a principle of the Gibbs energy minimization (15, 16). The program database contains the information about 17 000 substances. The program HSC Chemistry used in the given work is based on ideology of the European consortium SGTE (Scientific Group Thermodata Europe), which occupies with the development, support and distribution of high-quality databases. The SGTE structure includes specialized scientific centers in Germany, Canada, France, Sweden, the Great Britain and the USA (17). The subprogram "Equilibrium Compositions" is applied for the calculation of an equilibrium degree of elements' distribution in the investigated systems.

Kinetic research of the phosphorus extraction from ferrophosphorus at the presence of ferrosilicon was performed using an induction heating apparatus. An initial charge (100-110 g) was placed in a graphite crucible, which was put into the furnace and kept in a melting space of the furnace necessary time. Temperature in the furnace was measured by an optical pyrometer and a tungsten-rhenium thermocouple. After the experiment termination the crucible was taken from the furnace. A melt cooled in the crucible was weighed and analyzed on a phosphorus content using the technique (2). Some samples were analyzed using a scanning electron microscope JSM-6490LM (Japan), and also an x-ray diffractometer D8 Advance (Bruker). A degree of the phosphorus liberation in a gas phase (α_p , %) was calculated according to the results of the chemical analysis of the ferrophosphorus and the melt on a phosphorus content using the following equation:

$$\alpha_p = \frac{G_{FP} \cdot C_{P(FP)} - G_{melt} \cdot C_{P(melt)}}{G_{FP} \cdot C_{P(FP)}} \cdot 100; \quad (1)$$

where G_{FP} and G_{melt} – masses of the ferrophosphorus used and the melt produced accordingly, g;

$C_{P(FP)}$ and $C_{P(melt)}$ – a phosphorus content in the initial ferrophosphorus and in the melt accordingly, parts of unity.

At the experiment carrying out the electrothermal ferrophosphorus of the grade FeP 20-6 of the Limited Partnership "Kazphosphate" (Kazakhstan) was used, which has the following chemical composition: 26,4 % of P, 1,3 % of Si, 4,5 % of Mn, 66,0 % of Fe, 1,8 % - other, and also the ferrosilicon of the grade FS 65 (18) with the following composition: 63,8 % of Si, 0,6 % of Mn, 1,1 % of Al, 33,1 % of Fe, other – 1,4 %. The experimental data were processed using the equation:

$$\alpha = 1 - \exp[-k \cdot \tau^n], \quad (2)$$

where k and n – empirical coefficients, τ – duration of the process, minutes, α – degree of realization of the process, parts of unity. A speed of the process (V) (according to the IUPAC recommendations (20) as a speed of changing a degree of realization of a process,) was determined on the basis of the formula $V = d\alpha/d\tau$. In our case, a speed of the phosphorus liberation from the ferrophosphorus was calculated by means of differentiation of the equation (2) (21):

$$V = \frac{d\alpha}{d\tau} = n \cdot k^{1/n} \cdot \left[-\ln(1 - \alpha)^{1 - \frac{1}{n}} \right] \cdot (1 - \alpha). \quad (3)$$

The equation (7) allows us to estimate V for every value of α_p if "n" and "k" are known.

For the calculation of apparent activation energy of the process (E_{ap}) according to (22-23) we determined the dependence $\lg V = f(1/\tau)$ for fixed values α_p . Then E_{ap} was estimated under the formula:

$$E_{ap} = 2,303 \cdot 8,314 \cdot |tg\varphi| \quad (4)$$

where φ – inclination of the line to the abscissa axis; 8,314 – the universal gas constant, J/(mole*K); E_{ap} – apparent activation energy, J/mole.

Optimum technological parameters were determined by means of the fulfillment of the researches using the method of rotoTable planning of a second-order experiment, the development of adequate regression equation and the graphic optimization of the process by use of horizontal sections of the response surfaces (22).

3. Results and Their Discussion

3.1 Thermodynamic Analysis

For the system $\text{Fe}_3\text{P} - 3\text{FeSi}_2$ (the predicted reaction $\text{Fe}_3\text{P} + 3\text{FeSi}_2 = 6\text{FeSi} + 0,5\text{P}_2$) in a temperature interval of 500-2000°C the basic substances are FeP_2 , FeP , Fe_3P , P_4 , P_2 , FeSi , FeSi_2 , Fe_5Si_3 (Figure 1). In the system at 500°C 78 % of phosphorus transit in FeP_2 , 21,3 % - in FeP , the rest 0,7 % passes in Fe_3P . Thus the silicon is distributed in the following way: 79,4 % - in FeSi , and 20,6 % remain in FeSi_2 .

The beginning (1 %) of the formation of a gaseous phosphorus as P_4 and P_2 in the system is observed at 1110°C. The transformation of all the phosphorus in the gaseous P_2 , P_4 ($\alpha_{\text{P(gas)}}$) takes place at 1800°C (at 1700°C $\alpha_{\text{P(gas)}}$ makes 96,7 %). Most probably, the observed formation of FeP_2 and FeP in the system $\text{Fe}_3\text{P} - 3\text{FeSi}_2$ is connected with the reactions:

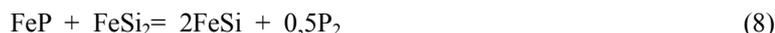


On the basis of the ΔG_r^0 calculation these reactions are possible at $T \geq 500^\circ\text{C}$ (Table 1).

Table 1. Temperature effect on ΔG_r^0 (kJ/mol of Fe_3P) of FeP_2 and FeP formation from Fe_2P

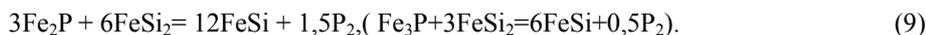
Reaction	Temperature, °C				
	500	700	900	1100	1300
5	-14,11	-14,88	-15,80	-16,91	-18,26
6	-11,36	-12,01	-12,84	-13,91	-15,29

Then, on the second stage the FeP_2 and FeP formed react with FeSi_2 :

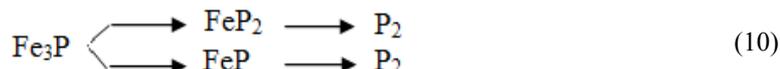


For these reactions temperatures of the beginning are 1252°C and 1122°C accordingly.

Summarily the reactions 5-8 lead to the reaction:



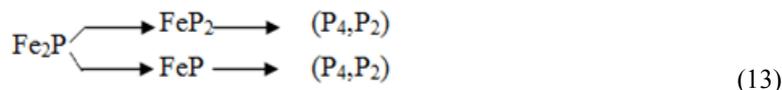
Thereby the chemical conversion in the system (concerning the phosphorus) occurs under the scheme:



In the system $\text{Fe}_2\text{P} - 2\text{FeSi}_2$ (the predicted reaction $\text{Fe}_2\text{P} + 2\text{FeSi}_2 = 4\text{FeSi} + 0,5\text{P}_2$) temperature of the beginning (1 %) of the gaseous phosphorus formation decreases from 1110°C to 1089°C. Formation of FeP and Fe_2P in the given system is a result of the reactions:



So, ΔG_r^0 of the reaction (11) at 500°C makes -11,91 kJ/mol of Fe_2P , at 900°C it makes -13,28 kJ/mol of Fe_2P , and ΔG_r^0 for the reaction (12) is -122 kJ/mol of Fe_2P and -13,8 kJ/mol of Fe_2P accordingly. Then, at the temperature above 1089°C there is the formation of P_2 owing to the reactions (7, 8). Conversion of all the phosphorus in a gaseous condition takes place at 1800°C (Figure 1). That is the phosphorus conversion in the system occurs according to the scheme:



In the system $\text{FeP} - \text{FeSi}_2$ (the predicted reaction $\text{FeP} + \text{FeSi}_2 = 2\text{FeSi} + 0,5\text{P}_2$) the formation of FeP_2 and FeSi (Figure 2) is a consequence of the reaction:



On the basis of calculation of ΔG_r^0 this reaction is possible already at 100°C (Table 2).

Table 2. Temperature effect on ΔG_r^0 (kJ/mol of FeP) of the reaction (14)

$T, ^{\circ}\text{C}$	100	300	500	700	900	1000	1100	1300
ΔG_r^0	-2,435	-2,598	-2,748	-2,871	-2,953	-2,978	-2,951	-2,991

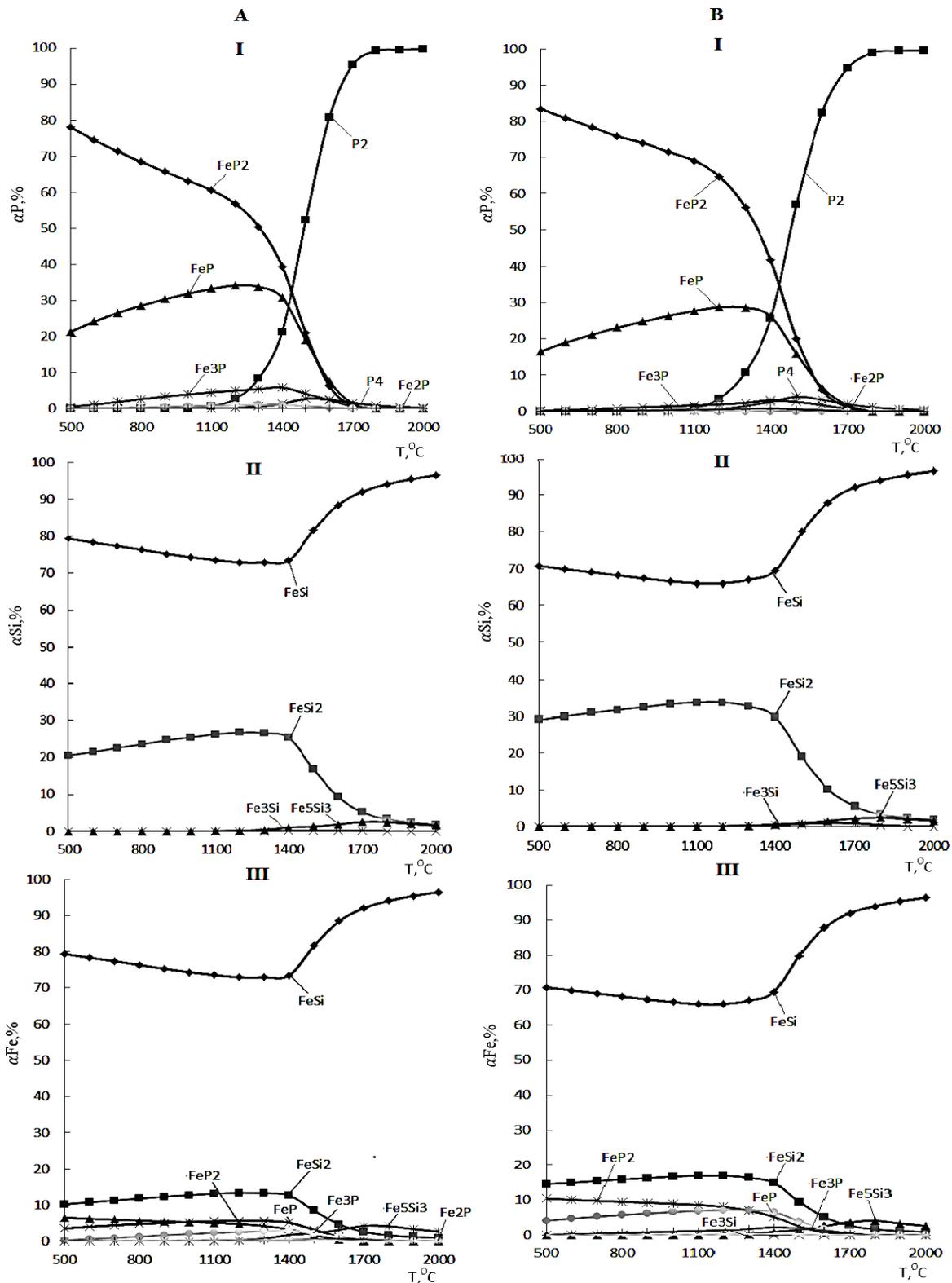
In this system 1 % of the P_2 formation occurs at 1017°C , and the full conversion – at 1800°C (at 1700°C α_{Pr} makes 98,5 %). A chemical reaction is the following:



For the system $\text{FeP}_2 - \text{FeSi}_2$ (the predicted reaction $\text{FeP}_2 + \text{FeSi}_2 = 2\text{FeSi} + \text{P}_2$) a temperature of the 1 % formation of the phosphorus is 519°C , and transition of all the phosphorus in the gas phase takes place at 1800°C (Figure 2).

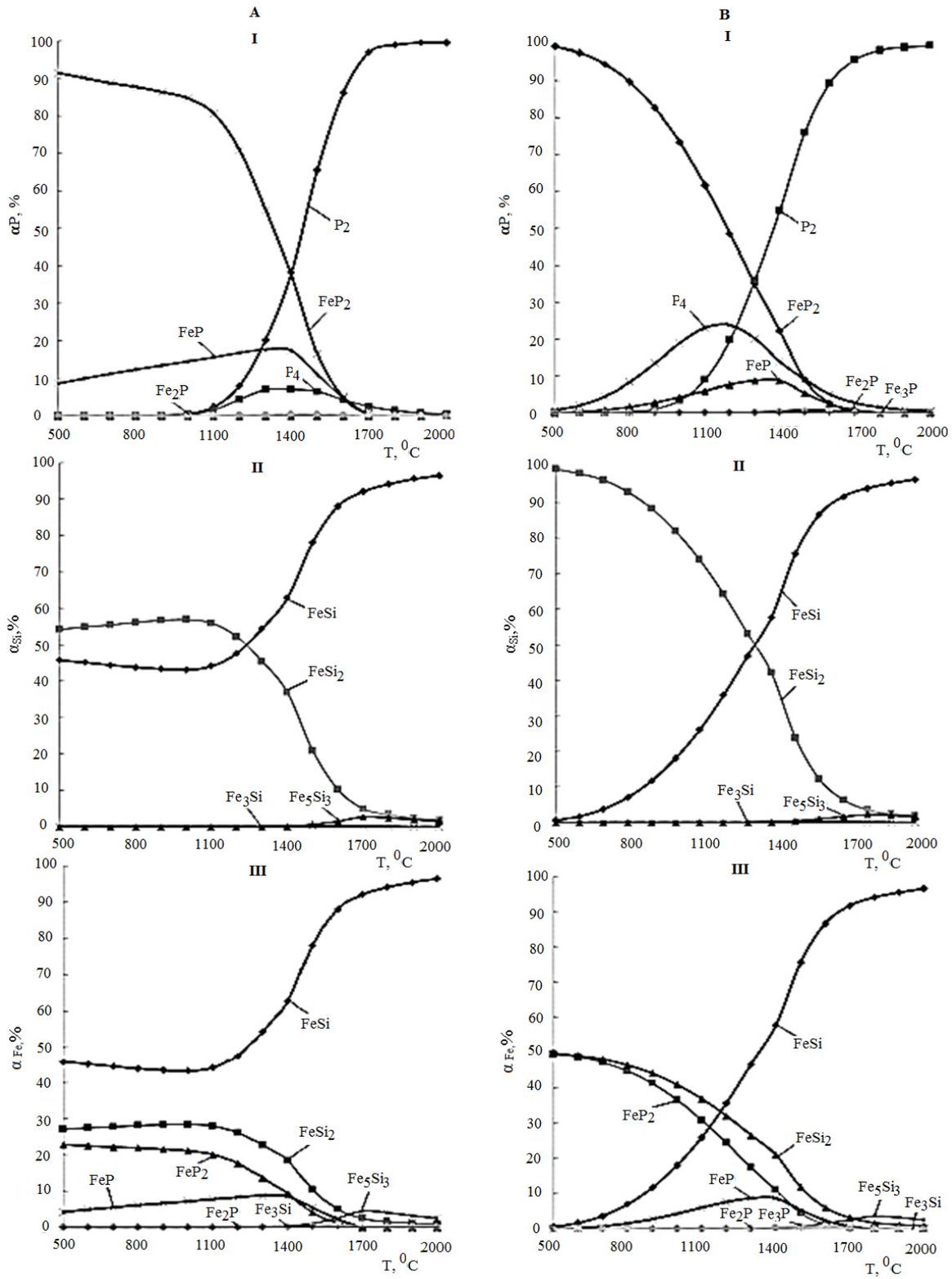
These researches allow us to define laws of the chemical interaction in the systems iron phosphides – FeSi_2 . So, a temperature of the 1 % formation of the gaseous phosphorus (T_1) depends on an atomic fraction of phosphorus in the iron phosphides (P_{phos}), decreasing from 1113°C to 519°C at increase P_{phos} from 25 % to 66,67 % (Table 3) according to the equation:

$$T_1 = 0,5166P_{\text{phos}} + 65,501. \quad (16)$$



A – the system $Fe_3P - FeSi_2$, B – the system $Fe_2P - FeSi_2$ I – P, II – Si, III – Fe

Figure 1. Temperature effect on an equilibrium degree (α) of the P, Si and Fe distribution in the systems $Fe_3P - FeSi_2$, $Fe_2P - FeSi_2$ at pressure 0,1MPa



A – the system FeP – FeSi₂, B – the system FeP₂ – FeSi₂, I – P, II – Si, III – Fe

Figure 2. Temperature effect on an equilibrium degree of P, Si and Fe distribution in the systems FeP – FeSi₂, FeP₂ – FeSi₂ at pressure 0,1MPa

Increase of P_{phos} also positively influences on α_{Pr} at high temperatures (Table 3).

Table 3. Influence of a mole fraction of phosphorus in iron phosphide (P_{phos}) on the temperature of 1 % phosphorus formation (T1) and α_{Pr}

P_{phos} , %	25,0	33,33	50,0	66,67
T1, °C	1119,0	1089,0	1017,0	519,0
$\alpha_{\text{Pr}}(1600^{\circ}\text{C})$, %	83,3	85,5	90,2	95,9
$\alpha_{\text{Pr}}(1700^{\circ}\text{C})$, %	96,7	97,0	98,5	99,4

3.2 Kinetics of the Process

Researches of kinetics of the phosphorus extraction in a gas phase at the chemical interaction of the ferrophosphorus, containing 26,4 % of phosphorus (FP), with the ferrosilicon of the grade FS 65, containing 63,8 % of silicon (FS), were fulfilled in a temperature interval of 1873-2073K. It was preliminary established, that a FS/FP ratio (γ) makes a significant impact on α_{P} (Table 4). In the further experiences γ is equal 2,4.

Table 4. Influence of a FS/FP ratio on α_{P} at the melting of a charge during 120 minutes and 1973K

γ	1,1	1,6	1,8	2,0	2,2	2,4	2,6
α_{P} , %	44,3	60,5	63,8	67,2	69,4	70,6	70,9

Influence of the melting process's temperature and duration on α_{P} is represented on the Figure 3.

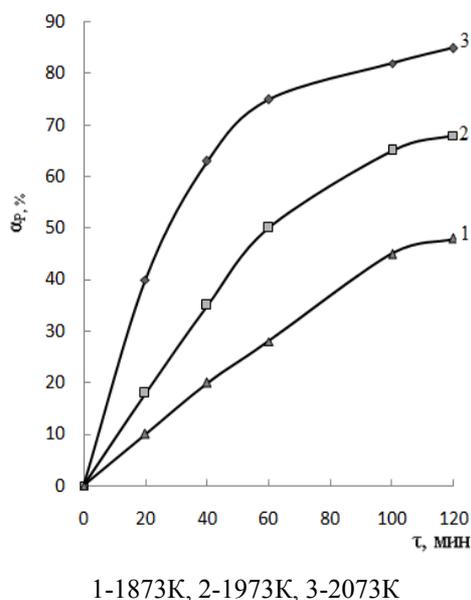


Figure 3. Influence of temperature and duration of the melting process on a degree of the gaseous phosphorus formation (α_{P}) in the system FP – γ FS at $\gamma = 2,4$

The Figure 3 shows that a considerable α_{P} (80-83 %) can be reach at 2073K within 100-120 minutes. Thus the ferrosilicon is formed which contains 44,6 % of Si, 48,8 % of Fe, 1,7 % of P, 1,9 % of Mn and 3 % of other (Figure 4).

Temperature influence on the parameters «n» and «k» in the equation (6) is represented in the Figure 6. The dependence equations $n = f(T)$ and $k = f(T)$ look in the following way:

$$n = 4,1554 - 0,00165 * T, \quad (17)$$

$$k = -3,5649 + 0,4729 \cdot \ln T. \tag{18}$$

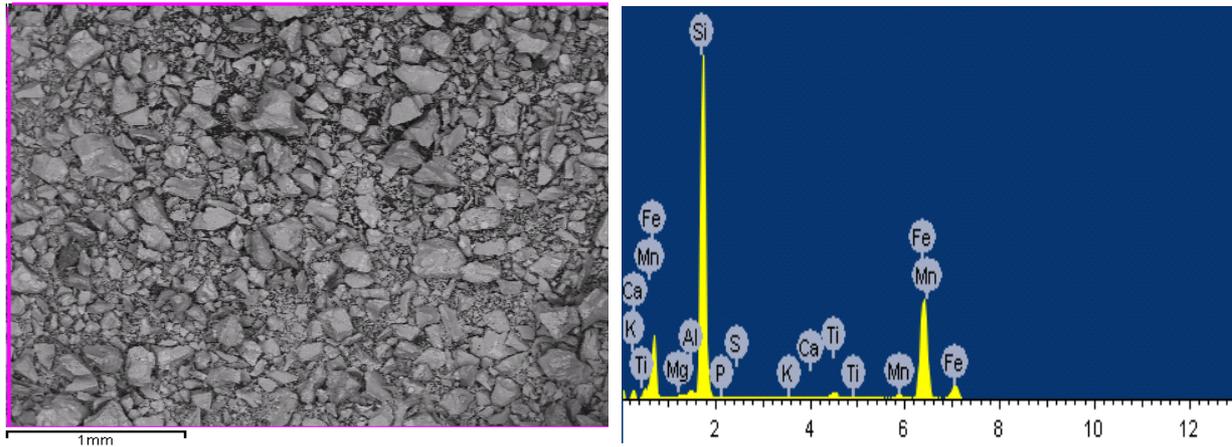
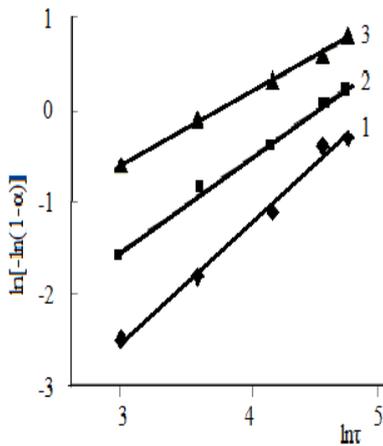


Figure 4. Electron microscopy of the ferrosilicon formed

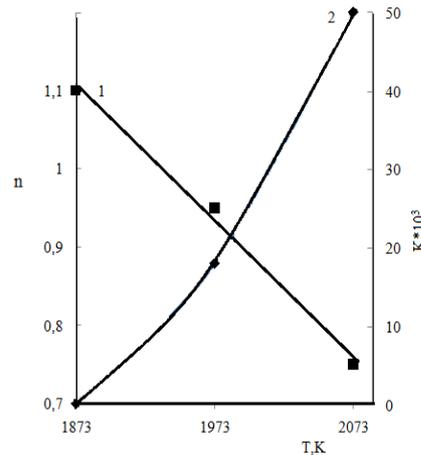
Applicability of the equation (2) to the process of phosphorus extraction from the ferrophosphorus is shown on the Figure 6.



1 – 1873K, 2 – 1973K, 3 – 2073K

Figure 5. Dependence

$\ln[-\ln(1 - \alpha)] = f(\ln\tau)$ at the extraction of phosphorus from the system FP – 2,4FS



1 - $n=f(T)$, 2 - $k=f(T)$

Figure 6. Temperature influence on the parameters «n» and «k» of the equation (6) at the extraction of phosphorus from the system FP – 2,4FS

Substituting the equations (17, 18) in the equation (2) we have established the generalized dependence $\alpha_p = f(T, \tau)$:

$$\alpha = 1 - \exp[(3,5649 - 0,4729) \cdot \tau^{(4,1514 - 16,5 \cdot 10^{-4} \cdot T)}] \tag{19}$$

After the differentiation of the equation (19) we have received the following expression for the phosphorus extraction rate (V):

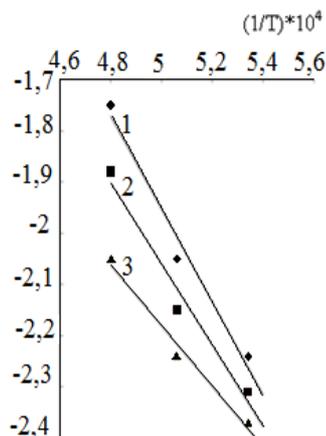
$$V = \frac{d\alpha}{d\tau} = (4,1554 - 16,5 \cdot 10^{-4} \cdot T) \cdot (0,4729 \cdot \ln T - 3,5649)^{\frac{1}{4,1554 - 16,5 \cdot 10^{-4} \cdot T} - 1} \cdot [-\ln(1 - \alpha)]^{1 - \frac{1}{4,1554 - 16,5 \cdot 10^{-4} \cdot T}} \cdot (1 - \alpha) \tag{20}$$

Using the equation (20), rates of the phosphorus extraction from the system FP – 2,4FS for $\alpha = 0,2, 0,3$ and $0,4$ were determined (Table 5).

Table 5. Influence of temperature and α_p on the phosphorus extraction rate (V) from the system FP – 2,4FS

Temperature, K	V, parts of unity/minute		
	$\alpha=0,2$	$\alpha=0,3$	$\alpha=0,4$
1873	0,00161	0,00146	0,00129
1973	0,0129	0,0104	0,009
2073	0,0177	0,0120	0,007

The temperature effect on V in coordinates $\lg V_p = f(1/T)$ is represented in the Figure 7. On the basis of this figure, using the equation (3), we detected that E_{ap} depends from α_p , reducing at the α_p decrease (Table 6).



1 – $\alpha_p = 20\%$, 2 – $\alpha_p = 30\%$, 4 – $\alpha_p = 40\%$

Figure 7. Dependence $\lg V_p = f(1/T)$ at the extraction of phosphorus from the system FP – 2,4FSTable 6. Influence of α_p on an apparent activation energy of the phosphorus liberation from the system FP – 2,4FS

$\alpha_p, \%$	20	30	40
$E_{ap}, \text{kJ/mol}$	389	325	281

Proceeding from the values E_{ap} received follows, that the process of phosphorus extraction from ferrophosphorus in the presence of ferrosilicon FS 65 takes place in kinetic area, and the decrease of E_{ap} at the increase of α_p is a consequence of intensification of influence of mass exchange phenomena on the process. Nevertheless the process intensification demands the temperature increase.

3.3 Determination of Optimum Parameters

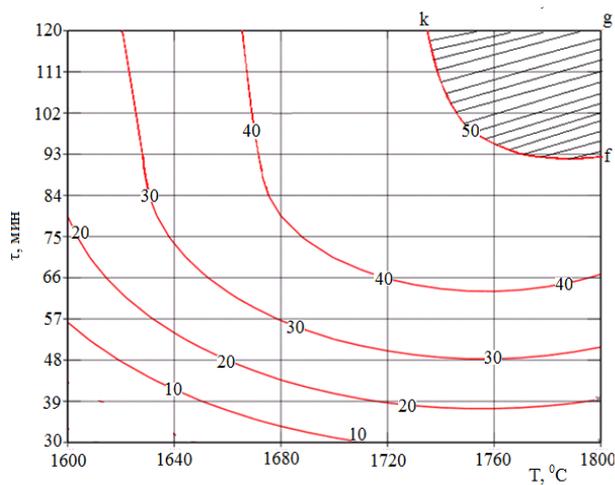
Independent variables are temperature (a coded kind – X1, a natural kind – T, °C), duration of the melting (a coded kind – X2, a natural one – τ , minutes) and a ratio of the ferrosilicon containing 63,8 % of Si to the ferrophosphorus containing 26,4 % P (a coded kind – X3, a natural one – γ). A matrix of planning of experiments for the determination of influence of T, τ and γ on degree of the phosphorus extraction in a gas phase ($\alpha_{p(gas)}$) is represented in the Table 7. On the basis of the experimental data (Table 7) the following adequate regression equation $\alpha_{p(gas)} = f(T, \tau, \gamma)$ was received.

$$\alpha_{p(gas)} = -3218.859 + 3.62 \cdot T - 32.781 \cdot \gamma + 1.463 \cdot \tau + 0.075 \cdot T \cdot \gamma + 0.00013 \cdot T \cdot \tau + 0.005 \cdot \tau \cdot \gamma - 0.001 \cdot T^2 - 21.736 \cdot \gamma^2 - 0.09 \cdot \tau^2 \quad (21)$$

Table 7. Matrix of planning of experiments on the processing of the ferrophosphorus containing 26,4 % of phosphorus

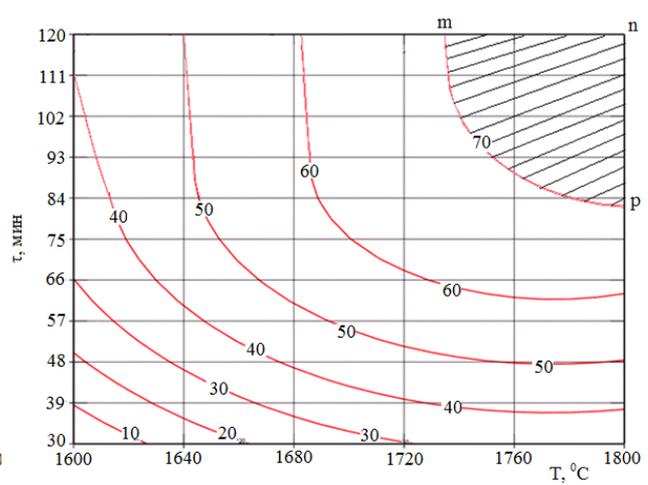
№	Variables			Variables			$\alpha_{P(gas)}, \%$	
	A coded kind			A natural kind			experim.	calcul.
	X1	X2	X3	T, °C	τ , min	γ		
1	2	3	4	5	6	7	8	9
1	1	1	1	1760	102	2,1	73.4	76.9
2	-1	1	1	1640	102	2,1	51.6	53.2
3	1	-1	1	1760	48	2,1	63.3	60
4	-1	-1	1	1640	48	2,1	39.6	36.3
5	1	1	-1	1760	102	1,1	44.0	46.9
6	-1	1	-1	1640	102	1,1	28.4	32.2
7	1	-1	-1	1760	48	1,1	31.4	29.9
8	-1	-1	-1	1640	48	1,1	19.5	15.2
9	1.6818	0	0	1800	75	1,6	66.4	65.2
10	-1.6818	0	0	1600	75	1,6	31.9	32.9
11	0	1.6818	0	1700	120	1,6	62.2	54.9
12	0	-1.6818	0	1700	30	1,6	19.3	26.4
13	0	0	1.6818	1700	75	2,4	65.4	66
14	0	0	-1.6818	1700	75	0,8	23.7	23
15	0	0	0	1700	75	1,6	59.5	59.8
16	0	0	0	1700	75	1,6	59.0	59.8
17	0	0	0	1700	75	1,6	58.3	59.8
18	0	0	0	1700	75	1,6	61.7	59.8
19	0	0	0	1700	75	1,6	60.4	59.8
20	0	0	0	1700	75	1,6	60.8	59.8

On the basis of the equation (21) we constructed a response surface and its horizontal sections (Figures 8-11).



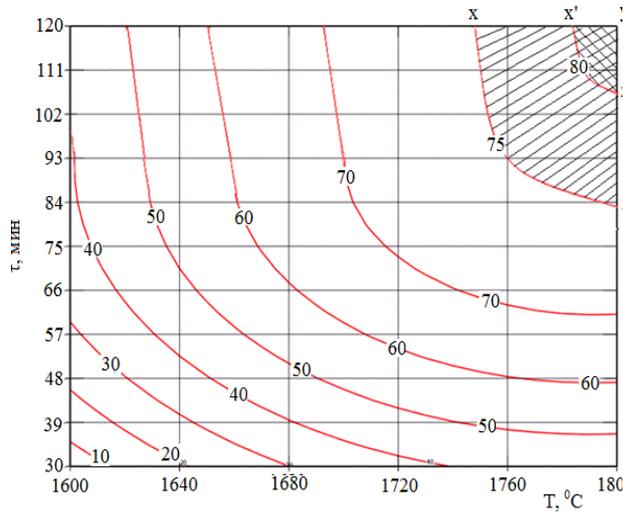
Numerals on lines – $\alpha_{P(gas)}, \%$

Figure 8. Horizontal sections of a response surface ($\alpha_{P(gas)}$) at the melting of ferrophosphorus (P = 26,4%) with ferrosilicon FS65, $\gamma = 1,1$



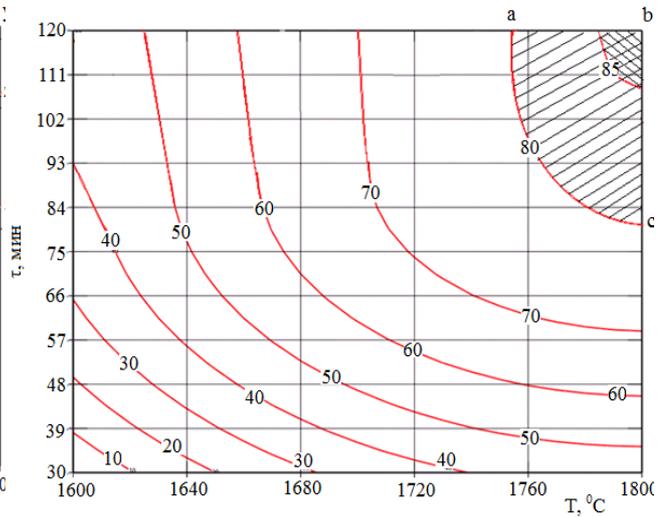
Numerals on lines – $\alpha_{P(gas)}, \%$

Figure 9. Horizontal sections of a response surface ($\alpha_{P(gas)}$) at the melting of ferrophosphorus (P = 26,4%) with ferrosilicon FS65, $\gamma = 1,6$



Numerals on lines – $\alpha_{p(gas)}, \%$

Figure 10. Horizontal sections of a response surface ($\alpha_{p(gas)}$) at the melting of ferrophosphorus (P = 26,4%) with ferrosilicon FS65, $\gamma = 2,1$



Numerals on lines – $\alpha_{p(gas)}, \%$

Figure 11. Horizontal sections of a response surface ($\alpha_{p(gas)}$) at the melting of ferrophosphorus (P = 26,4%) with ferrosilicon FS65, $\gamma = 2,4$

As follows from the figures 8 and 9, the processing the ferrophosphorus, containing 26,4 % of phosphorus, is noneffective at $\gamma = 1,1$. In this case $\alpha_{p(gas)}$ makes 50-54,8 % (the area kgf, the Figure 8). At the increasing γ to 1,6, $\alpha_{p(gas)}$ rises to 70-75 % (the area mnp, the Figure 9). A high ($> 80 \%$) $\alpha_{p(gas)}$ can be reached at $\gamma = 2,1$. However, the technological area x'y'z' (the Figure 10) is very narrow ($T = 1790-1800^{\circ}C$ and $\tau = 108-120$ min). At $\gamma = 2,4$ $\alpha_{p(gas)}$ reaches 80-86 % (the area abc, the Figure 11, $T = 1755-1800^{\circ}C$ and $\tau = 84-120$ min). A ferroalloy formed in this case contains 43,02 % of Si; 39,11 % of Fe; 2,57 % of Mn; 2,05 % of P, the Figure 12. Such complex ferroalloy (an addition alloy) can be used for melting foundry irons of grades J11-J16 containing 0,08-0,1 % of P, 1,2-3,6 % of Si, 0,5-1,0 % of Mn (23), and also a heat-resistant grey cast iron (P – 0,05-1,0 %, Si – 1-3 %, Mn - 0,25-1,0 %) and a malleable cast iron (P – to 0,18 %, Mn – 0,2-1,0 %, Si – 1,1-1,6 %) (24).

Element	Weight, %
Al	1,85
Si	43,02
P	9,05
Ca	0,23
Ti	0,56
V	0,22
Cr	0,37
Mn	2,57
Fe	39,11

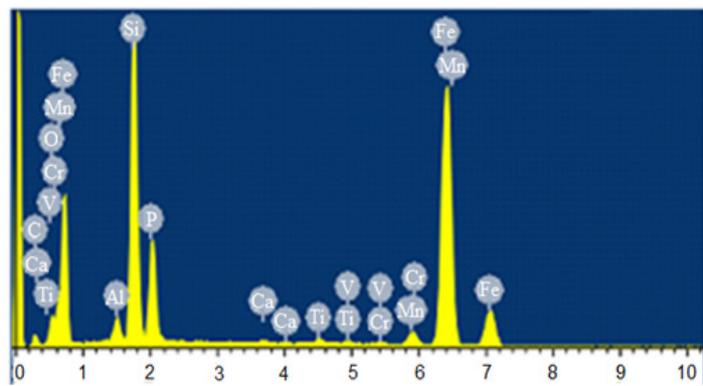


Figure 12. Electron microphotography and elemental composition of the ferroalloy produced at the melting the ferrophosphorus containing 26,4 % of P; $T = 1800^{\circ}C$; duration of the process is 100 min; $\gamma = 2,4$

4. Conclusions

On the basis of the experiments' results in the field of theory and technology of the processing ferrophosphorus in the presence of iron silicates it is possible to draw the following conclusions:

- At low temperatures ($500-700^{\circ}C$) in the systems $Fe_3P - FeSi_2$, $Fe_2P - FeSi_2$ and $FeP - FeSi_2$ there is the

saturation of iron phosphides by phosphorus and the formation of intermediate products FeP_2 and FeP , which react with the FeSi_2 at increase of temperature and form a gaseous phosphorus (as P_2 , P_4), i.e. the phosphorus liberation occurs through stages $\text{Fe}_3\text{P} \rightarrow \text{Fe}_2\text{P} \rightarrow \text{FeP} \rightarrow \text{FeP}_2 \rightarrow (\text{P}_2, \text{P}_4)$.

- A temperature of initial and final stages of the phosphorus formation in systems iron phosphides – FeSi_2 depends on an atomic content of phosphorus in a phosphide. At the increase of an atomic phosphorus content from 25 to 66,67 %, an initial temperature of the phosphorus formation decreases from 1110⁰C to 519⁰C, and the transition of the phosphorus in a gaseous state increases. A temperature of the full conversion of all the phosphorus in a gaseous state decreases at the increase of a mole ratio $\text{FeSi}_2/\text{Fe}_2\text{P}$. If a mole ratio $\text{FeSi}_2/\text{Fe}_2\text{P}$ raises from 2 to 3,2, then a temperature of the full transition of the phosphorus in a gaseous state decreases from 1800 to 1400⁰C.
- The phosphorus extraction from the ferrophosphorus in the presence of the ferrosilicon FS65 takes place in kinetic area, and the decrease of E_{ap} in the process is a consequence of the growth of influence of mass exchange phenomena. For intensification of the process it is necessary to increase the process temperature.
- a high degree (80-86 %) of the phosphorus extraction from the ferrophosphorus, containing 26,4 % of P, is observed at 1755-1800⁰C during 84-120 minutes and a mole ratio ferrosilicon FS65:ferrophosphorus equal 2,4. A complex ferroalloy formed in this case (an addition alloy), containing 43,02 % of Si; 2,57 % of Mn, 2,05 % of P, 39,11 % of Fe, can be used at melting foundry irons, including heat-resistant and malleable cast irons.

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